Problem 1 - 1.5, 1.6, 2.1a, 2.3 from the B&F text:

1.5 Use equation (1) from page 15 of the text and the knowledge that the double-layer charging is 6 pts 95% complete when t = 3τ . The table below gives the correct answers:

 $\tau = R_s C_d$

	t _{95%}	τ	R _s	C _d
	6 µs	2 µs	1Ω	2 μF
2 pts for	60 µs	20 µs	10 Ω	2 μF
correct	600 μs	200 µs	100 Ω	2 μF
numbers				
and units				

(1)

1.6 Use equation 1.2.15 from the text which describes the current during a potential sweep:

$$i = vC_d [1 - e^{-t/\tau}]$$

The assumption that we can neglect transients means that we can assume $t > \tau$, which gives equation (2) which describes the steady-state current (p 17 of B&F):

$$i \approx v C_d$$
 (2)

4 pts for the equation

4 pts for the equation

Using the value of $C_d = 2 \mu F$, we get:

Sweep rate (V/s)	Current (A)	
0.02	4 x 10 ⁻⁸	
1	2 x 10 ⁻⁶	2 pts for correct numbers
20	4 x 10 ⁻⁵	and units

2.1 (a) There are at least two acceptable solutions to this problem. The first is:

 $E^0 = -0.828 V$ $2H_2O + 2e^- \rightleftharpoons H_2 + 2OH^ H_2 \rightleftharpoons 2e^- + 2H^+$ $E^0 = 0.000 V$ $2H_20 \rightleftharpoons 2H^+ + 20H^ E^0 = -0.828 V$ Alternatively, $E^0 = -1.229 V$ $2H_20 \rightleftharpoons 0_2 + 4H^+ + 4e^-$

> $E^0 = 0.401 V$ $0_2 + 2H_20 + 4e^- \rightleftharpoons 40H^-$ E⁰ = -0.828 V $4H_20 \rightleftharpoons 4H^+ + 4e^-$

6 points for writing two balanced half-reactions that add up to the desired net reaction

4 points for the correct cell potential

14 pts

6 pts

One cell that can accomplish this is:

Pt/H⁺,Cl⁻/H₂//Na⁺,OH⁻/H₂/Pt

Another is:

To answer the questions at the bottom of the problem, we first see that the two half-reactions are given above. The overall cell potential is negative, which means that ΔG will be positive. Therefore the reaction is non-spontaneous and this will need to be an electrolytic cell for the reaction to go from left to right. Thus, the cathode will be negative.

2.3 Again, there may be more than one valid answer to this problem. Here is one:

18 points

$Na^+ + e^- \rightleftharpoons Na(s)$ $2Cl^- \rightleftharpoons Cl_2(g) + 2e^-$	E ⁰ = -2.714 V E ⁰ = -1.3583 V	6 pts for writing two balanced half- reactions that add	
$2Na^+ + 2Cl^- \rightleftharpoons 2Na(s) + Cl_2(g)$	E ⁰ = -4.0723 V	up to the desired net reaction	up to the desired

We can calculate ΔG^0 for the reaction above from $\Delta G^0 = -nFE^0$. Then, using the standard free energy of formation for Na(Hg) (multiplied by 2 since we need 2 moles according to the balanced equation above), we can write:

 $\frac{2Na^{+} + 2Cl^{-} \rightleftharpoons 2Na(s) + Cl_{2}(g)}{2Na(s) \rightleftharpoons 2Na(Hg)} \qquad \Delta G^{0} = 786 \text{ kJ/mol} \qquad 4 \text{ pts for getting the} \\ \frac{\Delta G^{0} = -170 \text{ kJ/mol}}{\Delta G^{0} = -170 \text{ kJ/mol}} \qquad Correct \Delta G$

This does not complete the reaction given, but no value for equilibration between $Cl_2(aq)$ and $Cl_2(g)$ was given in the text, so we'll just assume that the reaction is not exergonic enough to make this reaction spontaneous. Thus the reaction is *not spontaneous*. A possible design for this cell would be:

$$C(graphite)/Cl_2, Cl^2, Na^+/Hg(Na)$$
 2 pts

Reaction(s) that should occur before this one, from a thermodynamic standpoint are the following:

2 pts for cell schematic2 pts for spontaneousor not and the rest ofthe questions

Although these reactions are clearly more thermodynamically favorable, we know from the lectures that hydrogen evolution from a mercury electrode is kinetically terrible – there is a large overpotential required for the formation of hydrogen from water at a Hg electrode, which allows the (spontaneous) reaction for the Na(Hg) to take place with good current efficiency over the water reduction reaction. Note we are not given any numbers here to know what B&F mean by "good" current efficiency.

The B&F text says this process could be used to make either Cl_2 gas or Na metal commercially (assuming you can separate the Na from the amalgam), and is in fact used in the commercial production of Cl_2 . As a by-product in the commercial process, we get solutions of NaOH – water is used to regenerate the Hg and NaOH results. This NaOH solution is apparently concentrated enough to also be commercially useful.

But, the wording of the question is whether the cell would have a "commercial value", which really is more of an economic question than an electrochemistry question. We really don't know what the efficiency is, or the value of the products, or cost of the power you have to put into the cell etc., so this part of the question was really not answerable with the information given.

2 pts for trying to answer these questions

Problem 2

26 pts

(a) If all of the free energy of the reaction is converted to electrical energy, then the cell could achieve an open-circuit voltage equal to the cell potential. In order to calculate the cell potential correctly, we must first determine the number of moles of electrons transferred in the net reaction. The following balanced reactions give us the number of electrons for the overall reaction:

$$\begin{array}{c} CH_3CH_2OH + 3H_2O \rightarrow 12H^+ + 12e^- + 2CO_2 \\ 3O_2 + 12H^+ + 12e^- \rightarrow 6H_2O \\ \hline CH_3CH_2OH + 3O_2 \rightarrow 3H_2O + 2CO_2 \end{array}$$

10 pts for correct VOC (if it's not correct, partial credit is split 6-4 between showing a balanced equation and using the correct equation for VOC)

Thus the reaction requires 12 moles of electrons for each mole of ethanol. We can now calculate the maximum open-circuit voltage. [Note: It's probably best to ignore the bit about "standard conditions" since the value of ΔG is not given under standard conditions and no indication is given of what conditions are being employed here.]

$$V_{OC} = E = \frac{-\Delta G}{nF} = 1.14 V$$

(b) We can use the Butler-Volmer equation:

 $i = i_0 [e^{-\alpha \eta f n} - e^{(1-\alpha)\eta f n}]$ 6 pts, (4 for correct equation plus 2 for an exchange current with correct number and unit)

Since we are at high overpotentials, one of the two exponential terms will be very close to zero. In this case, we have $\eta = E_{eq} = 0.5 - 1.14 = -0.64 \text{ V}$, T = 383 K, and we assume $\alpha = 0.5$. Solving for i₀ and using n = 12 above, we obtain (for a 1 cm² electrode):

$$i_0 = \frac{i}{e^{-\alpha\eta fn}} = 5.5 \times 10^{-52} \, A$$

This is a ridiculously small exchange current. That's because we used the value of n for the full reaction (12, from above), and that isn't the right value of n to use in the Tafel equation, which uses the n from

the rate-limiting electron-transfer step. But since we weren't told what the rate-limiting step is, we don't know the correct value of n. However, we were told in the text and lectures that n is typically more like 1 or 2, which will give us much more reasonable values for the exchange-current density:

n	i ₀ (A cm ⁻²)
1	1.2 x 10 ⁻⁵ A
2	7.5 x 10 ⁻¹⁰ A 5.5 x 10 ⁻⁵² A
12	5.5 x 10 ⁻⁵² A

4 points for the overpotential

(c) Since the total overpotential was -0.64 V, the overpotential associated with the ethanol electrode is therefore -0.24 V under the assumptions of this problem. Although it is tempting to ratio the overpotential to the current to obtain R_{CT} , we are not in the regime of low overpotential in this case. Thus, we will calculate what R_{CT} would be in the case of low overpotential using the value of i_0 , which is independent of overpotential. In Bard we find equation (3.4.13) which gives the value of the charge-transfer resistance for a one-electron reaction. Since we do not know how many electrons are involved in the rate-determining step, we can write:

$$R_{CT} = \frac{RT}{nFi_0}$$
6 points (4 for the equation, 2 for correct
number and units for R_{CT})

Note that we do not have the area of the electrode being used, which is needed to calculate resistance (since i_0 is a current density here). As an approximation, we will assume 1 cm² electrodes so that a resistance value can be calculated from the data given. In general, the resistance will be inversely proportional to the area of the electrode. Again we give different values of the resistance for common choices of n (recall that the choice of n also influences the value of i_0):

n	R _{CT} (Ω)
1	2.7x10 ³ Ω
2	$2.2 \times 10^7 \Omega$
12	5.0 x 10 ⁴⁸ Ω

Problem 3

24 pts

First we calculate the theoretical maximum energy:

$$10 g EtOH \times \frac{1 mol EtOH}{46.0694 g EtOH} \times \frac{1324 kJ}{mol EtOH} = 287 kJ$$

Next we calculate the total energy from the fuel-cell reaction at 0.5 V = 0.5 J/C:

$$10 g EtOH \times \frac{1 mol EtOH}{46.0694 g EtOH} \times \frac{12 mol e^-}{mol EtOH} \times \frac{96485 C}{mol e^-} \times \frac{0.5 J}{C} = 126 kJ$$

Thus, the energy-conversion efficiency of the direct ethanol fuel cell is:

$$efficiency = \frac{126 \ kJ}{287 \ kJ} = 43.7\%$$

12 points - divided 4 pts each among the 3 steps: calculate total energy, electrical energy, and efficiency

Since the way efficiency is lost in the steam-reforming process is unclear from the problem, we can either assume that 80% of the energy available in the ethanol is lost in this step (i.e. energy must be put into the system to make it go) or that the reaction does not give 100% yield, or some combination of the two. The end result will be the same since the steam-reforming step and the fuel cell are in series. Thus, we can calculate the total energy output of the process assuming 100% efficiency for steam reforming and multiply the final value by 0.8 to obtain the correct energy output. The following reactions are relevant in this case:

 $CH_3CH_2OH + 3H_2O \rightarrow 6H_2 + 2CO_2$ steam reforming

And for the H₂ fuel cell:

$$H_2 \rightleftharpoons 2H^+ + 2e^-$$

$$\frac{1}{2}O_2 + 2H^+ + 2e^- \rightleftharpoons H_2O$$

$$H_2 + \frac{1}{2}O_2 \rightarrow H_2O$$

12 pts - divided 3 pts each among getting the H_2 fuel cell equation, calculating total energy, electrical energy, and efficiency

Thus, we can calculate the energy output of the system assuming 100% efficiency in the steamreforming step:

$$10 \ g \ EtOH \times \frac{1 \ mol \ EtOH}{46.0694 \ g \ EtOH} \times \frac{6 \ mol \ H_2}{1 \ mol \ EtOH} \times \frac{2 \ mol \ e^-}{mol \ H_2} \times \frac{96485 \ C}{mol \ e^-} \times \frac{0.5 \ J}{C} = 126 \ kJ$$

We can see that this is the same number obtained for the direct ethanol fuel cell, which makes sense for a cell giving the same voltage, because the free energy is a state function, and therefore is the same no matter what intermediate steps you take along the reaction path. However, since the steam-reforming step is only 80% efficient, we multiply by 0.8 and find that the overall energy output of the system is only 100.5 kJ. Thus the efficiency of this process is 35% and the direct ethanol cell is actually more efficient in this case. The fact that the H₂ cell gives a higher current density makes it seem more efficiency at first glance, but it is running at the same voltage, so the energy of each electron harvested is exactly the same. Therefore, the inefficiency of the steam-reforming process reduces the overall energy efficiency.

6 pts for turning in a paper with your name on it